

ENGINEERING STANDARD

FOR

PROCESS DESIGN OF HOT OIL

AND

TEMPERED WATER CIRCUITS

ORIGINAL EDITION

MARCH 1996

This standard specification is reviewed and updated by the relevant technical committee on May 2003(1) and March. 2018(2). The approved modifications are included in the present issue of IPS.

FOREWORD

The Iranian Petroleum Standards (IPS) reflect the views of the Iranian Ministry of Petroleum and are intended for use in the oil and gas production facilities, oil refineries, chemical and petrochemical plants, gas handling and processing installations and other such facilities.

IPS are based on internationally acceptable standards and include selections from the items stipulated in the referenced standards. They are also supplemented by additional requirements and/or modifications based on the experience acquired by the Iranian Petroleum Industry and the local market availability. The options which are not specified in the text of the standards are itemized in data sheet/s, so that, the user can select his appropriate preferences therein.

The IPS standards are therefore expected to be sufficiently flexible so that the users can adapt these standards to their requirements. However, they may not cover every requirement of each project. For such cases, an addendum to IPS Standard shall be prepared by the user which elaborates the particular requirements of the user. This addendum together with the relevant IPS shall form the job specification for the specific project or work.

The IPS is reviewed and up-dated approximately every five years. Each standards are subject to amendment or withdrawal, if required, thus the latest edition of IPS shall be applicable

The users of IPS are therefore requested to send their views and comments, including any addendum prepared for particular cases to the following address. These comments and recommendations will be reviewed by the relevant technical committee and in case of approval will be incorporated in the next revision of the standard.

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GENERAL DEFINITIONS

Throughout this Standard the following definitions shall apply.

COMPANY :

Refers to one of the related and/or affiliated companies of the Iranian Ministry of Petroleum such as National Iranian Oil Company, National Iranian Gas Company, National Petrochemical Company and National Iranian Oil Refinery And Distribution Company.

PURCHASER :

Means the "Company" where this standard is a part of direct purchaser order by the "Company", and the "Contractor" where this Standard is a part of contract document.

VENDOR AND SUPPLIER:

Refers to firm or person who will supply and/or fabricate the equipment or material.

CONTRACTOR:

Refers to the persons, firm or company whose tender has been accepted by the company.

EXECUTOR :

Executor is the party which carries out all or part of construction and/or commissioning for the project.

INSPECTOR :

The Inspector referred to in this Standard is a person/persons or a body appointed in writing by the company for the inspection of fabrication and installation work.

SHALL:

Is used where a provision is mandatory.

SHOULD:

Is used where a provision is advisory only.

WILL:

Is normally used in connection with the action by the "Company" rather than by a contractor, supplier or vendor.

MAY:

Is used where a provision is completely discretionary.

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0. INTRODUCTION

The primary purpose of IPS standard specifications on "Process Design of General Heating & Cooling Systems" is to establish minimum requirements and design criteria needed in process design of the following standards:

STANDARD CODE**STANDARD TITLE**[IPS-E-PR-400](#)

"Process Design of Cooling Water Circuits"

[IPS-E-PR-410](#)

"Process Design of Hot Oil & Tempered Water Circuits"

[IPS-E-PR-420](#)

"Process Design of Heat Tracing and Winterizing"

This Engineering Standard Specification covers:

"PROCESS DESIGN OF HOT OIL & TEMPERED WATER CIRCUITS"

Thermal liquids are used for process heating and cooling in the form of liquid, vapor or a combination of both. In addition to steam, thermal liquid include, hot and tempered water, mercury, Na, K, Dowtherms A and E, molten salt mixtures, hot oils and many others, each of which can be used for a specified field of application and can operate in different temperature ranges.

1. SCOPE

This Standard Specification is intended to cover the minimum requirements and recommendations deemed necessary to be considered in process design of "Hot Oil" and "Tempered Water" systems.

The scope is covered in two parts as:

- Part I** "Process Design of Hot Oil System"
- Part II** "Process Design of Tempered Water System"

Note 1:

This standard specification is reviewed and updated by the relevant technical committee on May 2003. The approved modifications by T.C. were sent to IPS users as amendment No. 1 by circular No. 221 on May 2003. These modifications are included in the present issue of IPS.

Note 2:

This standard specification is reviewed and updated by the relevant technical committee on May 2003. The approved modifications by T.C. were sent to IPS users as amendment No. 2 by circular No. 476 on March 2018. These modifications are included in the present issue of IPS.

2. REFERENCES

Throughout this Standard the following dated and undated standards/codes are referred to. These referenced documents shall, to the extent specified herein, form a part of this standard. For dated references, the edition cited applies. The applicability of changes in dated references that occur after the cited date shall be mutually agreed upon by the Company and the Vendor. For undated references, the latest edition of the referenced documents (including any supplements and amendments) applies.

IPS (IRANIAN PETROLEUM STANDARDS)

- [IPS-E-PR-190](#) "Layout and Spacing"
- [IPS-E-PR-440](#) "Process Design of Piping Systems (Process Piping & Pipeline Sizing)"
- [IPS-E-PR-771](#) "Process Requirements of Heat Exchanging Equipment"
- [IPS-E-PR-785](#) "Process Design of Air Cooled Heat Exchangers (Air Coolers)"
- [IPS-E-PR-810](#) "Process Design of Furnaces"
- [IPS-E-PR-850](#) "Process Requirements of Vessels, Reactors and Separators"

API (AMERICAN PETROLEUM INSTITUTE)

- API 570 "Piping Inspection Code: In-Service Inspection, Repair, and Alteration of Piping System"
- API 610 "Centrifugal Pumps for Petroleum, Petrochemical and Natural Gas Industries"
- API 650 "Welded Tanks for Oil Storage"

ASME (THE AMERICAN SOCIETY OF MECHANICAL ENGINEERS)

"ASME Code", Section VIII, Division 1

HEAT TRANSFER FLUID SYSTEMS (Shell Grove of Companies - 2011)

3. DEFINITIONS AND TERMINOLOGY

Not particular definition is implemented.

4. SYMBOLS AND ABBREVIATIONS

ASME	=	The American Society of Mechanical Engineers
CWS	=	Cooling Water Supply
CWR	=	Cooling Water Return
DP	=	Differential Pressure
DT	=	Differential Temperature
FCV	=	Flow Control Valve
LHV	=	Lower Heating Value
LIC	=	Level Indicator Controller
LG	=	Level Gauge
OGP	=	Oil, Gas and Petrochemical
OD	=	Outside Diameter
PG	=	Pressure gauge Valve
PI	=	Pressure Indicator
TCV	=	Temperature Control Valve
TEMA	=	Tubular Exchanger Manufacturers Association, Inc
TI	=	Temperature Indicator
TIC	=	Temperature Indicator Controller
TT	=	Temperature Transmitter

5. UNITS

This standard is based on international system of units (SI), as per [IPS-E-GN-100](#), except where otherwise specified.

PART I
PROCESS DESIGN OF HOT OIL SYSTEM

6. PROCESS DESIGN OF HOT OIL SYSTEM

6.1 General

6.1.1 A simplified schematic of major components of a hot oil system is given in Fig. 1. The heat transfer medium is pumped through a fired heater to the heat exchanger and returns to the pump suction surge tank. In some cases a fired heater may be replaced by electrical sources or indirect fire heater by a waste heat source, such as the exhaust stack of a gas turbine.

6.1.2 While the system is ordered and designed as a packaged system, all necessary equipment such as ladders, and platforms, guards for moving parts, etc., shall be supplied as part of the package.

6.1.3 Indoor equipment shall be suitably protected against damage by infiltration of moisture and dust during plant operation, shutdown, wash down, and the use of fire protection equipment.

6.1.4 Outdoor equipment shall be similarly protected, and in addition, it shall be suitable for continuous operation when exposed to rain, snow or ice, high wind, humidity, dust, temperature extremes, and other severe weather conditions.

6.1.5 The system shall be laid out such that to make all equipment readily accessible for cleaning, removal of burners, replacement of filters, controls and other working parts and for adjustment and lubrication of parts requiring such attention. For similar reasons, the heater front and rear doors shall be hinged or deviated.

6.1.6 Maintenance tools specially designed for the equipment shall be furnished with the system.

6.1.7 Spare parts must be readily available. If a stock of parts is not maintained by the manufacturer, critical spare items shall be furnished with the system.

6.2 Advantages and Disadvantages of Hot Oils

6.2.1 Advantages

The advantages of hot oils are:

- Low vapor pressure at ambient temperature.
- Always liquid and easy to handle.
- Blended for a specific temperature range.
- Higher specific heat than normally occurring hydrocarbons.

6.2.2 Disadvantages

The disadvantages of hot oils include:

- Escaping vapors are environmentally undesirable.
- When overheated, the oils will oxidize and coke on the fire tube. Also, they can be ignited.
- Ethers if used, are expensive.
- Ethers are hygroscopic and must be kept dry.

6.3 Hot Oil Heater Application

These heaters furnish a heating bath 300°C or higher, which is hot enough for process applications such as dry desiccant or hydrocarbon recovery regeneration gas. Another less severe application is heavier hydrocarbon vaporization prior to injection into a gas pipeline to raise the heating value.

Manufactured heat transfer oils are blended for about 90-95°C operating range. For example, Fig. 2, gives typical heat transfer properties for a 150 to 300°C polyphenyl ether.

6.4 Design

The following features and criteria shall be considered in process design of each component of the hot oil system.

6.4.1 Heater design

6.4.1.1 Process design of the heater is critical for satisfactory operation. The heat transfer fluid must have sufficient velocity, generally 1.2 to 3 m/s, to avoid excessive film temperatures on the heater tubes.

6.4.1.2 Design and capacity of the heater should be limited so that the maximum film temperature does not exceed the maximum recommended operating temperature of the fluid.

6.4.1.3 Hot spot occurrence should be avoided, since it can lead to tube failure and fluid degradation.

6.4.1.4 The heater shall be rated for the specified output. Multiple identical units may also be employed for the designed total heat load, but care shall be taken in system design to ensure adequate and proportional flow through the heaters.

6.4.1.5 The preferred thermal efficiency of the heater to be 80% based on LHV of fuel. The contractor shall specify the expected and guaranteed values for the thermal efficiency and the basis for their estimation.

6.4.1.6 Based on total outside surface area of the firetube (s) and the return flue(s), the average heat flux shall not exceed 17.35 kJ/s.m². The flame characteristics and combustion chamber design shall ensure that the maximum heat flux at any point is limited to 23.66 kJ/s.m².

6.4.1.7 Heating medium (hot oil) shall clearly be specified and its discharge temperature from the heater shall be limited to a specified value, in data sheet.

6.4.1.8 Under normal operating conditions, the rise in heating medium temperature across the heater shall not exceed the allowable DT specified in the data sheet.

6.4.1.9 The heater shall be designed to give an efficient heater operation over the complete operating load range.

6.4.1.10 Each heater (in case the use of multi-heater units), shall have a self-supporting stack designed to carry the total exhaust under the maximum firing conditions.

6.4.1.11 In general reference should be made to [IPS-E-PR-810](#), "Process Design of Furnaces" for design of heater and auxiliary systems.

6.4.2 Firing system design

6.4.2.1 The hot oil heater shall be designed for a continuous and reliable operation.

6.4.2.2 The burner(s) shall be designed for a minimum of 120 percent of normal full load firing and be suitable for firing the specified fuels (oil, gas or both) without undue maintenance or adjustment.

6.4.2.3 In case of a forced-draft type heater the burner design shall incorporate air/fuel ratio system(s) to ensure complete combustion with minimum amount of excess air. The air/fuel ratio

system shall be effective throughout the burner firing range i.e., from low to high fire positions.

6.4.2.4 The burner nozzles and other parts exposed to the radiant heat of the combustion chamber shall be made from heat resisting alloy steel.

6.4.2.5 The burner fuel and air openings shall be arranged to provide suitable velocities for complete mixing resulting in efficient combustion of the fuel.

6.4.2.6 Each burner shall have observation ports to permit sighting and inspection of the flame.

6.4.2.7 Suitable ignitor(s) shall be provided for firing fuel oil or gas and shall be of adequate output to permit safe ignition of the fuel.

6.4.3 Combustion air fan design

In case of forced-draft type heater the following should be considered:

6.4.3.1 The fan shall be designed for maximum ambient temperature.

6.4.3.2 The fan(s), performance shall be stable over the complete firing range i.e., maximum firing down to shut off.

6.4.3.3 Inlet screens shall be provided at fan(s) inlet.

6.4.3.4 Combustion air fan(s) shall be sized to handle a minimum of 120 percent of the normal full quantity of combustion air.

6.4.3.5 Outlet ducts of air fan (s) shall have some equipment like damper(s) for adjustment of the amount of intake air to the heater.

6.4.4 Heater control and instrumentation

The heater package shall be provided with the following control and instrumentation as minimum:

a) Fuel gas/oil control system complete with:

- Pressure gauges in important locations;
- Pressure regulators;
- Pressure relief valves;
- Flow control valves(s) on heater inlet line;
- Strainers;
- Isolating valves.

b) Fuel gas/oil emergency shut-off valve.

c) Heater TIC (modulating type) for hot oil temperature control.

d) Heater manual control for fire regulation.

e) Temperature switches shall be supplied for the following alarm and shutdown functions:

- Hot oil high temperature alarm;
- Hot oil high high temperature shutdown;
- Hot oil low temperature alarm;
- Stack high temperature alarm;
- Fuel oil low temperature alarm.

f) Pressure switches shall be supplied for the following alarm and shutdown functions:

- Hot oil high pressure alarm;
- Hot oil low pressure alarm;

- *Fuel gas/oil high supply pressure alarm;
- *Fuel gas/oil high supply pressure shutdown;
- *Fuel gas/oil low supply pressure alarm;
- *Fuel gas low low supply pressure shutdown.

g) Flow switches installed on the flow transmitter output shall be supplied for the following functions:

- Turning Unit down to low flame position on low flow condition;
- Shutting Unit down (including circulation pumps) on low low flow condition.

h) Additionally, the following instrumentation shall be provided on the hot oil heater:

- Pressure gauge complete with isolation and bleed valve;
- Temperature indicators complete with thermowells for hot oil inlet and outlet streams;
- Stack exhaust temperature indicator complete with thermowell;
- ASME rated relief valve(s), factory set and sealed and located suitably. Relief valves shall have stainless steel trim.

i) Automatic start up/shutdown sequence control is normally not recommended, but if specified by the Company shall consist of:

- Pre-ignition purge of the combustion chamber;
- Ignition;
- Pilot proving;
- Firing rate modulation between low flame position and the maximum output;
- Post purge after shutdown.

j) The burner management system if specified by the Company shall be housed in a locally mounted panel, suitable for the area classification in which it is installed.

k) The burner management system shall incorporate a remote shutdown facility so that the main burner(s) and pilot(s) can be extinguished by a push-button located in central control room.

l) All other instrument, and controlling systems as per Vendor specification such as flame failure detector, pilot flame monitoring etc., should also be considered.

*** Pressure switches shall be installed on each fuel supply line.**

For exhaust gas instrumentation refer to appropriate standard.

6.4.5 Hot oil surge tank design

6.4.5.1 A surge tank shall be provided, suitably sized to handle expansion of inventory in whole system, the size of the expansion vessel is based upon the expansion coefficient, Maximum temperature and quantity of the fluid in the circuit and shall be designed as a pressure vessel in accordance with [IPS-E-PR-850](#).

6.4.5.2 The surge tank shall be arranged on the pump suction side and shall be blanketed with fuel gas or inert gas.

6.4.5.3 The surge tank shall be located inside the heater building.

6.4.5.4 The surge tank shall be provided complete with the following:

- a)** Level gauge(s), spanning the entire operating range.
- b)** Pressure gauge.
- c)** Pressure relief valve.

- d) Blanket gas pressure make-up regulator.
- e) Pressure regulator to vent tank over pressure due to expansion or filling.
- f) Make-Up connection complete with isolation valve and non-return valve.
- g) Level alarm high and low.

6.4.6 Circulating pump design

6.4.6.1 At least two centrifugal pumps (one operating and one stand by) with 10% over design capacity at the design head shall be provided. However the following requirement shall also be considered in design.

6.4.6.2 Strainer shall be provided at the suction of each pump.

6.4.6.3 Valving around each pump shall include the following:

- a) Suction isolation gate valve of the same size as the suction line.
- b) Non-Return valve in discharge line.
- c) Isolation gate valve in discharge line.
- d) Casing vent and drain valves.

6.4.6.4 In design of pump suction and discharge lines, the differential thermal expansion of the lines due to temperature variation shall be taken into account.

The stand-by pump shall be maintained in a pre-heated state in order to avoid thermal shock when starting by including a via bypass across the check valve.

6.4.7 Hot oil filter

6.4.7.1 A hot-oil filter shall be provided to handle a slipstream equal to 10% of the design flow rate.

6.4.7.2 The filter shall be of disposable cartridge type, capable of removing all solid particles above 5 micrometers (microns).

6.4.7.3 The hot-oil filter shall be provided complete with the following:

- a) DP gauge.
- b) Isolation valves at inlet and outlet.
- c) Restriction orifice, sized for the required flow rate.
- d) Vent and drain valves.
- e) Relief valve.
- f) Filter by-pass line.

6.4.8 Carbon filter

6.4.8.1 A bulk-pack type carbon absorber in consistent with the heating medium should be provided downstream of the heating medium filter to remove any products of degradation.

6.4.8.2 The design flow rate of carbon filter shall be the same as the hot-oil filter flow-rate.

6.4.8.3 The carbon filter shall be provided complete with the following:

- a) DP gauge.

- b) Isolation valves at inlet and outlet.
- c) Vent and drain valves.
- d) Relief valve.
- e) Filter by-pass line.

6.4.9 Piping

Piping shall be carbon steel unless otherwise specified. To minimize the possibility of leakage, the connections in Piping, fittings, and equipment should be welded.

6.5 Performance Guarantees

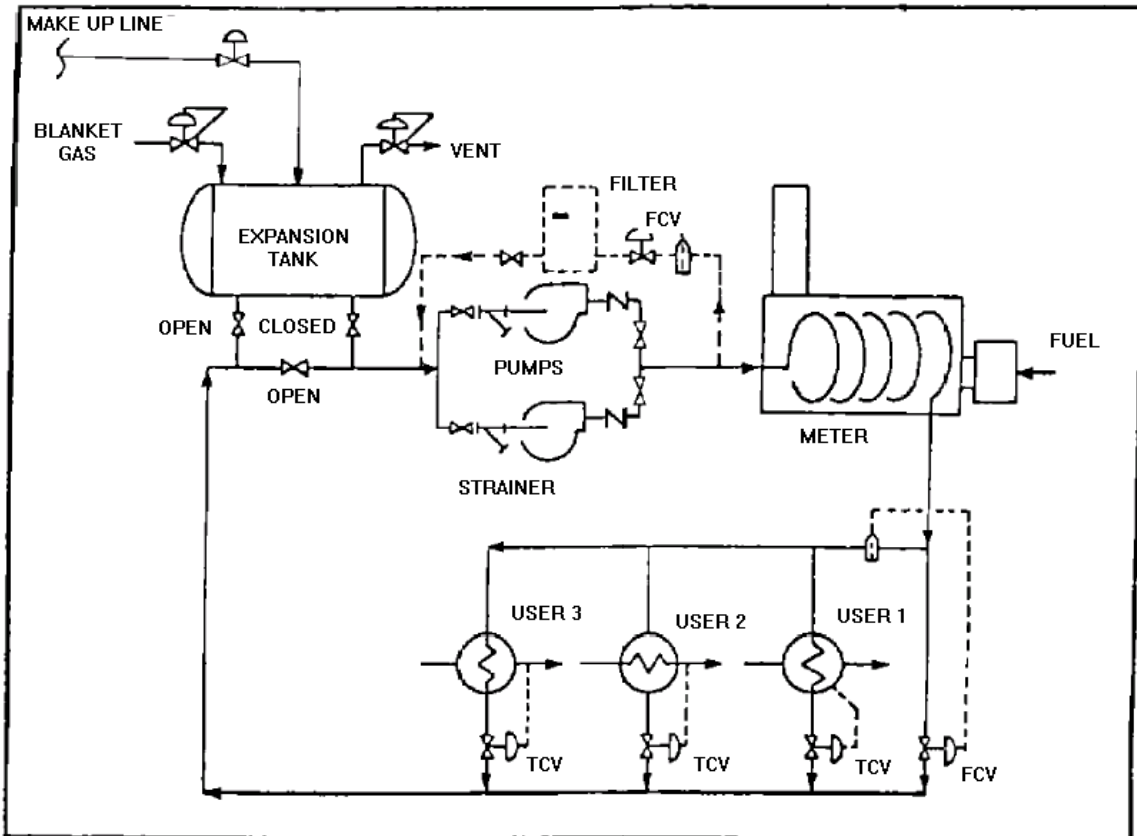
6.5.1 The Vendor, unless he expressly states any exceptions in his proposal, shall specify the guarantees on which the system furnished by him to meet the requirement with regard to process design, as flow rate, hot-oil delivery pressure and temperature, safety and reliability under all specified operating conditions. Refer to IPS-E-PR-250.

6.6 Specific Project Requirements

6.6.1 The Vendor shall specify the following data and information as the "Specific Project Requirements" in his proposal.

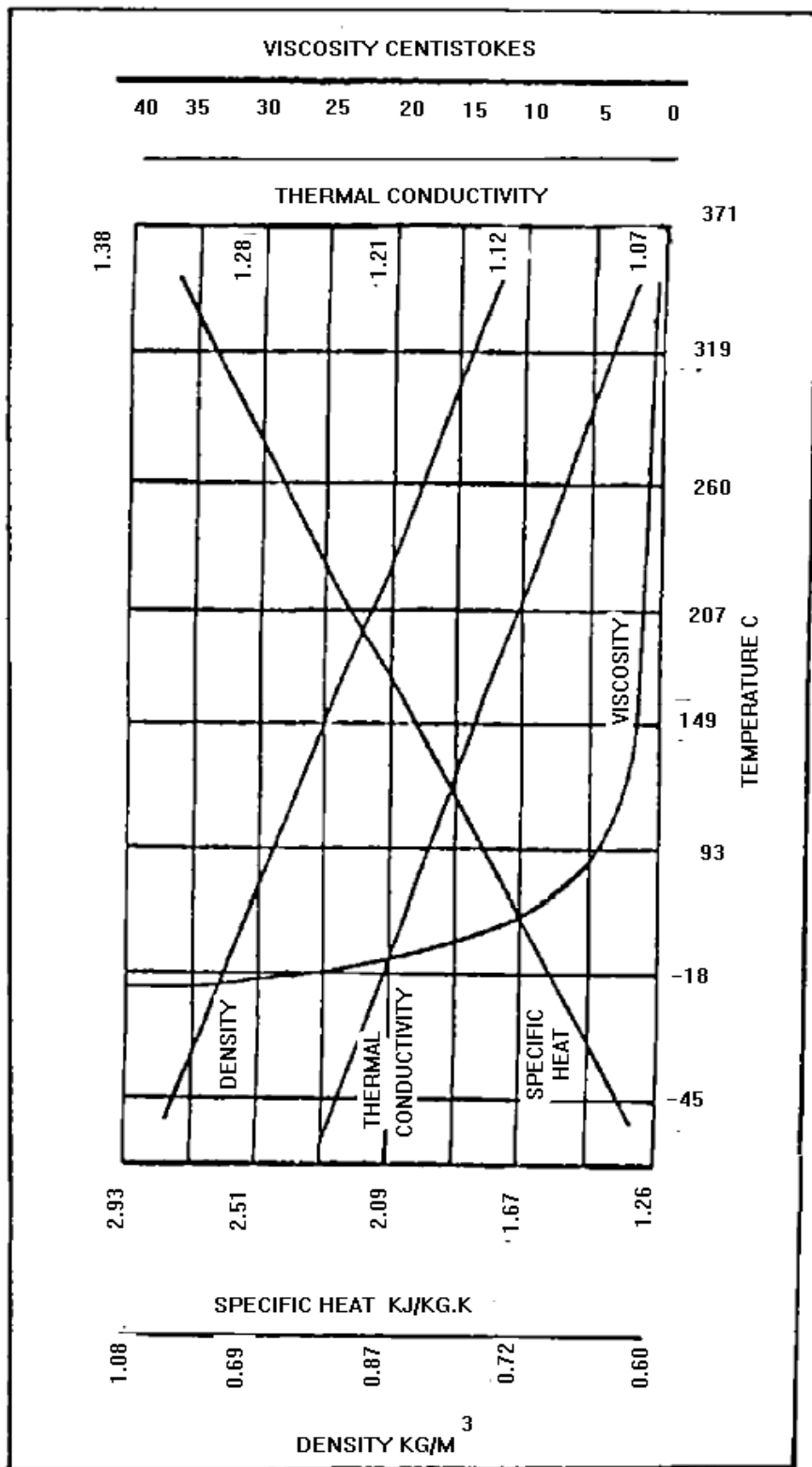
- Project:
- Location:Elevation m
- Environment: non-corrosive.....corrosive
- Barometric pressure..... kPa (abs)
- Heat transfer medium fluid
- Concentration:mass% in water
- Circulation rate:m³/h
- Pump differentialkPa
- Temperature of heat transfer fluid to heater: °C
- Temperature of heat transfer fluid from heater: °C
- Design circulation rate:m³/h
- Design pump differential:kPa
- Design temperature, heater outlet: °C
- Design, heater duty:MJ/h
- System Design pressure:kPa (ga)at °C
- Maximum pressure drop accross heater: kPa
- Surge tank:..... Required.....Not required
- Circulation pump:Required.....Not required
- Hot oil filter:Required.....Not required
- Carbon adsorber:Required.....Not required
- Supply header size:..... mm
- Return header size:.....mm
- System capacity, excluding heater package: m³
- Instrument air:Instrument gas
 - Supply pressure..... kPa (ga) normal
 - Design pressure kPa (ga) at °C
- Area classification:

- Fuel gas..... sweetsour
 - Supply pressurekPa (ga) normal
 - Design pressurekPa (ga) at °C
 - Relative density (specific gravity) (Air=1.0)..... Molecular mass (MW).....
- Composition:
-
-
-



TYPICAL HOT OIL SYSTEM

Fig. 1



TYPICAL HEAT TRANSFER PROPERTIES OF HOT OIL (POLYPHENYL ETHER)

Fig. 2

PART II
PROCESS DESIGN OF TEMPERED WATER SYSTEM

7. PROCESS DESIGN OF TEMPERED WATER SYSTEM

7.1 General

7.1.1 Using tempered water as a cooling medium for solutions that would freeze or crystallize at usual cooling water temperatures is a common practice.

7.1.2 A special tempered water circulating system shall be designed to minimize the chance of fouling by deposition of these type materials on heat exchanger surfaces.

7.1.3 Condensate or treated process water shall be used as circulating tempered water, the water should efficiently be treated for corrosion inhibition according to material specification and design procedures. Provisions for corrosion inhibitor facilities shall be made. Tempered water system typically consists of a surge drum, circulating pumps, air cooler and/or shell-tube heat exchanger and associated piping and measuring devices.

7.1.4 Single or multiple user(s) may be incorporated in a single tempered water system. All components of the system should accordingly be designed to maintain required cooling load capacity when all or parts of the user(s) are in operation.

7.1.5 The water return from the various users shall be cooled to specified temperature depending on the local climatic conditions.

7.1.6 All applicable parts of general requirements set forth in Clause 6, "Part I" of this Standard shall be considered for this part unless is in contrary with Vendor specification.

7.2 General Layout and Operational Facilities

7.2.1 For layout and operation of the system, Vendor should take into account an adequate space being allowed for operational access, cleaning and maintenance.

7.2.2 The arrangement of installations should be such that, instruments and indicators can readily be seen from the appropriate working position. Valves and controls should be neatly arranged and accessible.

7.2.3 In case the system admitted for indoor installation, access facilities should be so arranged that major items of the system can be brought in and taken out or removed as necessary.

7.2.4 Applicable provisions of [IPS-E-PR-190](#), should also be considered in system layout design by the Vendor.

7.3 Process Design Requirements

7.3.1 General

7.3.1.1 Design of the system and it's associated controls should take into account the following:

- a) The nature of the application.
- b) The type of installation i.e., indoor or outdoor installation.
- c) Cooling load patterns.

- d) Tempered water supply requirements.
- e) Economic factor and minimizing the use of primary energy.

7.3.2 Surge drum

7.3.2.1 The Pressurized type surge drums for required capacity shall be designed in accordance with [IPS-E-PR-850](#). Atmospheric surge tanks shall be designed as per API-650 with steam blanketing system for oxygen removal.

7.3.2.2 Make up water to surge drum will be taken from condensate system, moderately heated to required temperature by hot condensate circulation and chemical treatment should be practiced to minimize corrosion.

7.3.2.3 The drum should be blanketed with steam. Provisions shall be considered for automatic controlling of water level and adding make-up water as required.

7.3.2.4 The pressurized type surge drum operating above 7.0 kPa shall have a minimum design pressure of 110 kPa (abs). The drum shall be designed for full vacuum.

7.3.2.5 All applicable loads, including wind load, earthquake and hydrostatic testing load shall be considered in design as acting simultaneously.

7.3.2.6 All outline drawing shall be furnished and shall contain the data indicated in Table 1 below. Location of the drum marking or nameplate shall be indicated on this drawing.

TABLE 1 - DATA IN DRAWING

DESCRIPTION	UNIT	DATA
·Design pressure	kPa	----
·Design temperature	°C	----
·Operating pressure	kPa	----
·Operating temperature	°C	----
·Maximum allowable stress at design temperature	kPa	----
·Hydrostatic test pressure at uppermost part of drum	kPa (ga)	----
·Hydrostatic test temperature	°C	----

7.3.2.7 A manufacturer’s data report shall be furnished and shall contain the same information as required by form U-1 of ASME Code, Section VIII, Division 1.

7.3.2.8 Provisions for entering, cleaning, venting and draining of vessel shall be considered on the bases of basic practice as specified by the Vendor/manufacturer.

7.3.2.9 Surge drum shall be furnished with following auxiliaries:

- a) Pressure gauge.
- b) Temperature gauge.
- c) Level gauge.
- d) Steam blanketing regulator.
- e) All inlet, outlet piping nozzles.

7.3.3 Circulating/recirculating centrifugal pumps

7.3.3.1 The circulating and recirculating pumps shall be centrifugal with 100% spare and shall be designed in accordance with the following requirements:

- a) Unless otherwise specified, the pumps and auxiliaries shall be suitable for unsheltered

outdoor installation in the climatic zone specified.

- b) Flanged suction and discharge nozzles shall be integral with the casing.
- c) Gate valves shall be used for vents and drains.
- d) All required vents shall be equipped with valve.
- e) Nameplate data shall be in SI units.
- f) Vendor's piping shall terminate with a flanged or threaded connection, of a line rating at least equal to the design pressure and design temperature rating of the equipment.
- g) Vendor shall specify the spare parts and shall include his proposed method of protection from corrosion during shipment and subsequent storage.
- h) Vendor's proposal shall state the minimum flow rate recommended for sustained operation on the specified tempered water.
- i) Isolation gate valves shall be used at suction and discharge line with the same respective line size.
- j) Non-return valves shall be installed in discharge lines.

7.3.3.2 The pumps shall be of proven modern design and shall have operating characteristics as specified in pump data sheet.

7.3.3.3 The arrangement of equipment, including piping and auxiliaries shall provide adequate clearance area and safe access for operation and maintenance.

7.3.3.4 The equipment and component parts shall be warranted against defective materials, design and workmanship for specified guaranteed period.

7.3.4 Cooler and heat exchanger

7.3.4.1 Unless otherwise required, air cooler shall be used in tempered water system, in accordance with [IPS-E-PR-785](#).

7.3.4.2 In case shell-tube heat exchanger is required, its design shall be in accordance with [IPS-E-PR-771](#).

7.3.5 Piping design

7.3.5.1 All applicable portions of [IPS-E-PR-440](#) shall be considered in pipe sizing and design of the tempered water system. It shall apply to auxiliary piping connecting the equipment of the system and the piping between the system and the consuming Units. However, the following considerations shall be admitted to accomplish the whole requirements of piping process design.

- 1) In piping layout, the location of operating and control points such as valves, flanges, instruments, vents and drains shall enable operation of the system with minimum difficulties.
- 2) The piping system shall be laid out to allow easy repair or replacement of any portion of the system.
- 3) Basic design data for each line shall be given in the line designation table as per Company's project specification.
- 4) The actual minimum corrosion allowance shall be listed for each line in the line designation table.
- 5) Flanges or other removable connections shall be provided throughout the piping system to permit complete removal of the piping.
- 6) A gate valve shall be installed in each instrument take-off connection except thermowells and shall be located close to the pipe.

7) All piping connections to equipment shall be suitable for the equipment design and the hydraulic test pressure.

7.3.6 Other requirements

7.3.6.1 The whole system should be arranged and sized so that the design-cooling load can be met by an appropriate flow of tempered water within the applicable system temperature limits.

7.3.6.2 Circulating piping should be thermally insulated and traced where local climatic condition implies.

7.3.6.3 Isolating valves are normally fully open or fully shut and should be provided to facilitate isolation of individual items of equipment.

7.3.6.4 An appropriate and compatible automatic controls should be arranged for the system elements.

7.3.6.5 Proper study should be prepared for biocide or other additives and their monitoring.